

## Environmental Protection Agency

§ 63.9824

### OTHER REQUIREMENTS AND INFORMATION

#### § 63.9820 What parts of the General Provisions apply to me?

Table 11 to this subpart shows which parts of the General Provisions specified in §§63.1 through 63.15 apply to you.

#### § 63.9822 Who implements and enforces this subpart?

(a) This subpart can be implemented and enforced by us, the U.S. Environmental Protection Agency (U.S. EPA), or a delegated authority such as your State, local, or tribal agency. If the U.S. EPA Administrator has delegated authority to your State, local, or tribal agency, then that agency, in addition to the U.S. EPA, has the authority to implement and enforce this subpart. You should contact your U.S. EPA Regional Office to find out if implementation and enforcement to this subpart is delegated to your State, local, or tribal agency.

(b) In delegating implementation and enforcement authority to this subpart to a State, local, or tribal agency under 40 CFR part 63, subpart E, the authorities contained in paragraph (c) of this section are retained by the Administrator of the U.S. EPA and are not transferred to the State, local, or tribal agency.

(c) The authorities that cannot be delegated to State, local, or tribal agencies are as specified in paragraphs (c)(1) through (4) of this section.

(1) Approval of alternatives to the applicability requirements in §§63.9782 and 63.9784, the compliance date requirements in §63.9786, and the emission limitations in §63.9788.

(2) Approval of major changes to test methods under §63.7(e)(2)(ii) and (f) and as defined in §63.90.

(3) Approval of major changes to monitoring under §63.8(f) and as defined in §63.90.

(4) Approval of major changes to recordkeeping and reporting under §63.10(f) and as defined in §63.90.

#### § 63.9824 What definitions apply to this subpart?

Terms used in this subpart are defined in the Clean Air Act, in 40 CFR

63.2, the General Provisions of this part, and in this section as follows:

*Additive* means a minor addition of a chemical, mineral, or metallic substance that is added to a refractory mixture to facilitate processing or impart specific properties to the final refractory product.

*Add-on air pollution control device (APCD)* means equipment installed on a process vent that reduces the quantity of a pollutant that is emitted to the air.

*Autoclave* means a vessel that is used to impregnate fired and/or unfired refractory shapes with pitch to form pitch-impregnated refractory products. Autoclaves also can be used as defumers following the impregnation process.

*Bag leak detection system* means an instrument that is capable of monitoring particulate matter loadings in the exhaust of a fabric filter in order to detect bag failures. A bag leak detection system includes, but is not limited to, an instrument that operates on triboelectric, light-scattering, light-transmittance, or other effects to monitor relative PM loadings.

*Basket* means the metal container used to hold refractory shapes for pitch impregnation during the shape preheating, impregnation, defuming, and, if applicable, coking processes.

*Batch process* means a process in which a set of refractory shapes is acted upon as a single unit according to a predetermined schedule, during which none of the refractory shapes being processed are added or removed. A batch process does not operate continuously.

*Binder* means a substance added to a granular material to give it workability and green or dry strength.

*Catalytic oxidizer* means an add-on air pollution control device that is designed specifically to destroy organic compounds in a process exhaust gas stream by catalytic incineration. A catalytic oxidizer includes a bed of catalyst media through which the process exhaust stream passes to promote combustion and incineration at a lower temperature than would be possible without the catalyst.

*Chromium refractory product* means a refractory product that contains at least 1 percent chromium by weight.

*Clay refractory product* means a refractory product that contains at least 10 percent uncalcined clay by weight prior to firing in a kiln. In this definition, the term “clay” means any of the following six classifications of clay defined by the U.S. Geologic Survey: ball clay, bentonite, common clay and shale, fire clay, fuller’s earth, and kaolin.

*Coking oven* means a thermal process unit that operates at a peak temperature typically between 540° and 870 °C (1000° and 1600 °F) and is used to drive off the volatile constituents of pitch-impregnated refractory shapes under a reducing or oxygen-deprived atmosphere.

*Continuous parameter monitoring system (CPMS)* means the total equipment that is used to measure and record temperature, pressure, liquid flow rate, gas flow rate, or pH on a continuous basis in one or more locations. “Total equipment” includes the sensor, mechanical components, electronic components, data acquisition system, data recording system, electrical wiring, and other components of a CPMS.

*Continuous process* means a process that operates continuously. In a continuous process unit, the materials or shapes that are processed are either continuously charged (fed) to and discharged from the process unit, or are charged and discharged at regular time intervals without the process unit being shut down. Continuous thermal process units, such as tunnel kilns, generally include temperature zones that are maintained at relatively constant temperature and through which the materials or shapes being processed are conveyed continuously or at regular time intervals.

*Curing oven* means a thermal process unit that operates at a peak temperature typically between 90° and 340 °C (200° and 650 °F) and is used to activate a thermosetting resin, pitch, or other binder in refractory shapes. Curing ovens also perform the same function as shape dryers in removing the free moisture from refractory shapes.

*Defumer* means a process unit that is used for holding pitch-impregnated re-

fractory shapes as the shapes defume or cool immediately following the impregnation process. This definition includes autoclaves that are opened and exhausted to the atmosphere following an impregnation cycle and used for holding pitch-impregnated refractory shapes while the shapes defume or cool.

*Deviation* means any instance in which an affected source subject to this subpart, or an owner or operator of such a source:

(1) Fails to meet any requirement or obligation established by this subpart including, but not limited to, any emission limitation (emission limit, operating limit, or work practice standard);

(2) Fails to meet any term or condition that is adopted to implement an applicable requirement in this subpart for any affected source required to obtain such a permit; or

(3) Fails to meet any emission limitation (emission limit, operating limit, or work practice standard) in this subpart during startup, shutdown, or malfunction, regardless of whether or not such failure is permitted by this subpart.

*Dry injection fabric filter (DIFF)* means an add-on air pollution control device that includes continuous injection of hydrated lime or other sorbent into a duct or reaction chamber followed by a fabric filter.

*Dry lime scrubber/fabric filter (DLS/FF)* means an add-on air pollution control device that includes continuous injection of humidified hydrated lime or other sorbent into a reaction chamber followed by a fabric filter. These systems may include recirculation of some of the sorbent.

*Dry limestone adsorber (DLA)* means an air pollution control device that includes a limestone storage bin, a reaction chamber that is essentially a packed-tower filled with limestone, and may or may not include a peeling drum that mechanically scrapes reacted limestone to regenerate the stone for reuse.

*Emission limitation* means any restriction on the emissions a process unit may discharge.

*Fabric filter* means an add-on air pollution control device used to capture particulate matter by filtering a process exhaust stream through a filter or

filter media; a fabric filter is also known as a baghouse.

*Fired refractory shape* means a refractory shape that has been fired in a kiln.

*HAP* means any hazardous air pollutant that appears in section 112(b) of the Clean Air Act.

*Kiln* means a thermal process unit that operates at a peak temperature greater than 820 °C (1500 °F) and is used for firing or sintering refractory, ceramic, or other shapes.

*Kiln furniture* means any refractory shape that is used to hold, support, or position ceramic or refractory products in a kiln during the firing process.

*Maximum organic HAP processing rate* means the combination of process and refractory product formulation that has the greatest potential to emit organic HAP. The maximum organic HAP processing rate is a function of the organic HAP processing rate, process operating temperature, and other process operating parameters that affect emissions of organic HAP. (See also the definition of *organic HAP processing rate*.)

*Organic HAP processing rate* means the rate at which the mass of organic HAP materials contained in refractory shapes are processed in an affected thermal process unit. The organic HAP processing rate is a function of the amount of organic HAP contained in the resins, binders, and additives used in a refractory mix; the amounts of those resins, binders, and additives in the refractory mix; and the rate at which the refractory shapes formed from the refractory mix are processed in an affected thermal process unit. For continuous process units, the organic HAP processing rate is expressed in units of mass of organic HAP per unit of time (*e.g.*, pounds per hour). For batch process units, the organic HAP processing rate is expressed in units of mass of organic HAP per unit mass of refractory shapes processed during the batch process cycle (*e.g.*, pounds per ton).

*Particulate matter (PM)* means, for the purposes of this subpart, emissions of particulate matter that serve as a measure of total particulate emissions as measured by EPA Method 5 of 40 CFR part 60, appendix A.

*Peak emissions period* means the period of consecutive hourly mass emissions of the applicable pollutant that is greater than any other period of consecutive hourly mass emissions for the same pollutant over the course of a specified batch process cycle, as defined in paragraphs (1) and (2) of this definition. The peak emissions period is a function of the rate at which the temperature of the refractory shapes is increased, the mass and loading configuration of the shapes in the process unit, the constituents of the refractory mix, and the type of pollutants emitted.

(1) The 3-hour peak THC emissions period is the period of 3 consecutive hours over which the sum of the hourly THC mass emissions rates is greater than the sum of the hourly THC mass emissions rates for any other period of 3 consecutive hours during the same batch process cycle.

(2) The 3-hour peak HF emissions period is the period of 3 consecutive hours over which the sum of the hourly HF mass emissions rates is greater than the sum of the hourly HF mass emissions rates for any other period of 3 consecutive hours during the same batch process cycle.

*Period of natural gas curtailment or supply interruption* means a period of time during which the supply of natural gas to an affected facility is halted for reasons beyond the control of the facility. An increase in the cost or unit price of natural gas does not constitute a period of natural gas curtailment or supply interruption.

*Pitch* means the residue from the distillation of petroleum or coal tar.

*Pitch-bonded refractory product* means a formed refractory product that is manufactured using pitch as a bonding agent. Pitch-bonded refractory products are manufactured by mixing pitch with magnesium oxide, graphite, alumina, silicon carbide, silica, or other refractory raw materials, and forming the mix into shapes. After forming, pitch-bonded refractory products are cured in a curing oven and may be subsequently fired in a kiln.

*Pitch-impregnated refractory product* means a refractory shape that has been fired in a kiln, then impregnated with heated coal tar or petroleum pitch

under pressure. After impregnation, pitch-impregnated refractory shapes may undergo the coking process in a coking oven. The total carbon content of a pitch-impregnated refractory product is less than 50 percent.

*Pitch working tank* means a tank that is used for heating pitch to the impregnation temperature, typically between 150° and 260 °C (300° and 500 °F); temporarily storing heated pitch between impregnation cycles; and transferring pitch to and from the autoclave during the impregnation step in manufacturing pitch-impregnated refractory products.

*Plant site* means all contiguous or adjoining property that is under common control, including properties that are separated only by a road or other public right-of-way. Common control includes properties that are owned, leased, or operated by the same entity, parent entity, subsidiary, or any combination thereof.

*Redundant sensor* means a second sensor or a back-up sensor that is integrated into a CPMS and is used to check the parameter value (e.g., temperature, pressure) measured by the primary sensor of the CPMS.

*Refractory product* means nonmetallic materials containing less than 50 percent carbon by weight and having those chemical and physical properties that make them applicable for structures, or as components of systems, that are exposed to environments above 538 °C (1000 °F). This definition includes, but is not limited to: refractory bricks, kiln furniture, crucibles, refractory ceramic fiber, and other materials used as linings for boilers, kilns, and other processing units and equipment where extremes of temperature, corrosion, and abrasion would destroy other materials.

*Refractory products that use organic HAP* means resin-bonded refractory products, pitch-bonded refractory products, and other refractory products that are produced using a substance that is an organic HAP, that releases an organic HAP during production of the refractory product, or that contains an organic HAP, such as methanol or ethylene glycol.

*Refractory shape* means any refractory piece forming a stable mass with specific dimensions.

*Research and development process unit* means any process unit whose purpose is to conduct research and development for new processes and products and is not engaged in the manufacture of products for commercial sale, except in a de minimis manner.

*Resin-bonded refractory product* means a formed refractory product that is manufactured using a phenolic resin or other type of thermosetting resin as a bonding agent. Resin-bonded refractory products are manufactured by mixing resin with alumina, magnesium oxide, graphite, silica, zirconia, or other refractory raw materials, and forming the mix into shapes. After forming, resin-bonded refractory products are cured in a curing oven and may be subsequently fired in a kiln.

*Responsible official* means one of the following:

(1) For a corporation: a president, secretary, treasurer, or vice-president of the corporation in charge of a principal business function, or any other person who performs similar policy or decisionmaking functions for the corporation, or a duly authorized representative of such person if the representative is responsible for the overall operation of one or more manufacturing, production, or operating facilities applying for or subject to a permit and either:

(i) The facilities employ more than 250 persons or have gross annual sales or expenditures exceeding \$25 million (in second quarter 1980 dollars); or

(ii) The delegation of authority to such representatives is approved in advance by the Administrator;

(2) For a partnership or sole proprietorship: a general partner or the proprietor, respectively;

(3) For a municipality, State, Federal, or other public agency: either a principal executive officer or ranking elected official. For the purposes of this part, a principal executive officer of a Federal agency includes the chief executive officer having responsibility for the overall operations of a principal geographic unit of the agency (e.g., a Regional Administrator of EPA); or

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(4) For affected sources (as defined in this subpart) applying for or subject to a title V permit: "responsible official" shall have the same meaning as defined in part 70 or Federal title V regulations in this chapter (42 U.S.C. 7661), whichever is applicable.

*Shape dryer* means a thermal process unit that operates at a peak temperature typically between 40° and 700 °C (100° and 1300 °F) and is used exclusively to reduce the free moisture content of a refractory shape. Shape dryers generally are the initial thermal process step following the forming step in refractory products manufacturing. (See also the definition of a *curing oven*.)

*Shape preheater* means a thermal process unit that operates at a peak temperature typically between 180° and 320 °C (350° and 600 °F) and is used to heat fired refractory shapes prior to

the impregnation step in manufacturing pitch-impregnated refractory products.

*Thermal oxidizer* means an add-on air pollution control device that includes one or more combustion chambers and is designed specifically to destroy organic compounds in a process exhaust gas stream by incineration.

*Uncalcined clay* means clay that has not undergone thermal processing in a calciner.

*Wet scrubber* means an add-on air pollution control device that removes pollutants from a gas stream by bringing them into contact with a liquid, typically water.

*Work practice standard* means any design, equipment, work practice, or operational standard, or combination thereof, that is promulgated pursuant to section 112(h) of the Clean Air Act.

TABLE 1 TO SUBPART SSSSS OF PART 63—EMISSION LIMITS

As stated in §63.9788, you must comply with the emission limits for affected sources in the following table:

For . . .	You must meet the following emission limits . . .
1. Each new or existing curing oven, shape dryer, and kiln that is used to process refractory products that use organic HAP; each new or existing coking oven and defumer that is used to produce pitch-impregnated refractory products; each new shape preheater that is used to produce pitch-impregnated refractory products; AND each new or existing process unit that is exhausted to a thermal or catalytic oxidizer that also controls emissions from an affected shape preheater or pitch working tank.	As specified in items 2 through 9 of this table.
2. Continuous process units that are controlled with a thermal or catalytic oxidizer.	a. The 3-hour block average THC concentration must not exceed 20 parts per million by volume, dry basis (ppmvd), corrected to 18 percent oxygen, at the outlet of the control device; or b. The 3-hour block average THC mass emissions rate must be reduced by at least 95 percent.
3. Continuous process units that are equipped with a control device other than a thermal or catalytic oxidizer.	a. The 3-hour block average THC concentration must not exceed 20 ppmvd, corrected to 18 percent oxygen, at the outlet of the control device; or b. The 3-hour block average THC mass emissions rate must be reduced by at least 95 percent.
4. Continuous process units that use process changes to reduce organic HAP emissions.	The 3-hour block average THC concentration must not exceed 20 ppmvd, corrected to 18 percent oxygen, at the outlet of the process gas stream.
5. Continuous kilns that are not equipped with a control device	The 3-hour block average THC concentration must not exceed 20 ppmvd, corrected to 18 percent oxygen, at the outlet of the process gas stream.
6. Batch process units that are controlled with a thermal or catalytic oxidizer.	a. The 2-run block average THC concentration for the 3-hour peak emissions period must not exceed 20 ppmvd, corrected to 18 percent oxygen, at the outlet of the control device; or b. The 2-run block average THC mass emissions rate for the 3-hour peak emissions period must be reduced by at least 95 percent.
7. Batch process units that are equipped with a control device other than a thermal or catalytic oxidizer.	a. The 2-run block average THC concentration for the 3-hour peak emissions period must not exceed 20 ppmvd, corrected to 18 percent oxygen, at the outlet of the control device; or

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For . . .	You must meet the following emission limits . . .
8. Batch process units that use process changes to reduce organic HAP emissions.	b. The 2-run block average THC mass emissions rate for the 3-hour peak emissions period must be reduced by at least 95 percent. The 2-run block average THC concentration for the 3-hour peak emissions period must not exceed 20 ppmvd, corrected to 18 percent oxygen, at the outlet of the process gas stream.
9. Batch process kilns that are not equipped with a control device.	The 2-run block average THC concentration for the 3-hour peak emissions period must not exceed 20 ppmvd, corrected to 18 percent oxygen, at the outlet of the process gas stream.
10. Each new continuous kiln that is used to produce clay refractory products.	a. The 3-hour block average HF emissions must not exceed 0.019 kilograms per megagram (kg/Mg) (0.038 pounds per ton (lb/ton)) of uncalcined clay processed, OR the 3-hour block average HF mass emissions rate must be reduced by at least 90 percent; and b. The 3-hour block average HCl emissions must not exceed 0.091 kg/Mg (0.18 lb/ton) of uncalcined clay processed, OR the 3-hour block average HCl mass emissions rate must be reduced by at least 30 percent.
11. Each new batch process kiln that is used to produce clay refractory products.	a. The 2-run block average HF mass emissions rate for the 3-hour peak emissions period must be reduced by at least 90 percent; and b. The 2-run block average HCl mass emissions rate for the 3-hour peak emissions period must be reduced by at least 30 percent.

TABLE 2 TO SUBPART SSSSS OF PART 63—OPERATING LIMITS

As stated in §63.9788, you must comply with the operating limits for affected sources in the following table:]

For . . .	You must . . .
1. Each affected source listed in Table 1 to this subpart .....	a. Operate all affected sources according to the requirements to this subpart on and after the date on which the initial performance test is conducted or required to be conducted, whichever date is earlier; and b. Capture emissions and vent them through a closed system; and c. Operate each control device that is required to comply with this subpart on each affected source during all periods that the source is operating, except where specified in §63.9792(e), item 2 of this table, and item 13 of Table 4 to this subpart; and d. Record all operating parameters specified in Table 8 to this subpart for the affected source; and e. Prepare and implement a written OM&M plan as specified in §63.9792(d).
2. Each affected continuous kiln that is equipped with an emission control device.	a. Receive approval from the Administrator before taking the control device on the affected kiln out of service for scheduled maintenance, as specified in §63.9792(e); and b. Minimize HAP emissions from the affected kiln during all periods of scheduled maintenance of the kiln control device when the kiln is operating and the control device is out of service; and c. Minimize the duration of all periods of scheduled maintenance of the kiln control device when the kiln is operating and the control device is out of service.
3. Each new or existing curing oven, shape dryer, and kiln that is used to process refractory products that use organic HAP; each new or existing coking oven and defumer that is used to produce pitch-impregnated refractory products; each new shape preheater that is used to produce pitch-impregnated refractory products; AND each new or existing process unit that is exhausted to a thermal or catalytic oxidizer that also controls emissions from an affected shape preheater or pitch working tank.	Satisfy the applicable operating limits specified in items 4 through 9 of this table.
4. Each affected continuous process unit .....	Maintain the 3-hour block average organic HAP processing rate (pounds per hour) at or below the maximum organic HAP processing rate established during the most recent performance test.

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For . . .	You must . . .
5. Continuous process units that are equipped with a thermal oxidizer.	Maintain the 3-hour block average operating temperature in the thermal oxidizer combustion chamber at or above the minimum allowable operating temperature for the oxidizer established during the most recent performance test.
6. Continuous process units that are equipped with a catalytic oxidizer.	<ul style="list-style-type: none"> <li>a. Maintain the 3-hour block average operating temperature at the inlet of the catalyst bed of the oxidizer at or above the minimum allowable operating temperature for the oxidizer established during the most recent performance test; and</li> <li>b. Check the activity level of the catalyst at least every 12 months.</li> </ul>
7. Each affected batch process unit .....	For each batch cycle, maintain the organic HAP processing rate (pounds per batch) at or below the maximum organic HAP processing rate established during the most recent performance test.
8. Batch process units that are equipped with a thermal oxidizer.	<ul style="list-style-type: none"> <li>a. From the start of each batch cycle until 3 hours have passed since the process unit reached maximum temperature, maintain the hourly average operating temperature in the thermal oxidizer combustion chamber at or above the minimum allowable operating temperature established for the corresponding period during the most recent performance test, as determined according to item 11 of Table 4 to this subpart; and</li> <li>b. For each subsequent hour of the batch cycle, maintain the hourly average operating temperature in the thermal oxidizer combustion chamber at or above the minimum allowable operating temperature established for the corresponding hour during the most recent performance test, as specified in item 13 of Table 4 to this subpart.</li> </ul>
9. Batch process units that are equipped with a catalytic oxidizer.	<ul style="list-style-type: none"> <li>a. From the start of each batch cycle until 3 hours have passed since the process unit reached maximum temperature, maintain the hourly average operating temperature at the inlet of the catalyst bed at or above the minimum allowable operating temperature established for the corresponding period during the most recent performance test, as determined according to item 12 of Table 4 to this subpart; and</li> <li>b. For each subsequent hour of the batch cycle, maintain the hourly average operating temperature at the inlet of the catalyst bed at or above the minimum allowable operating temperature established for the corresponding hour during the most recent performance test, as specified in item 13 of Table 4 to this subpart; and</li> <li>c. Check the activity level of the catalyst at least every 12 months.</li> </ul>
10. Each new kiln that is used to process clay refractory products.	Satisfy the applicable operating limits specified in items 11 through 13 of this table.
11. Each affected kiln that is equipped with a DLA .....	<ul style="list-style-type: none"> <li>a. Maintain the 3-hour block average pressure drop across the DLA at or above the minimum levels established during the most recent performance test; and</li> <li>b. Maintain free-flowing limestone in the feed hopper, silo, and DLA at all times; and</li> <li>c. Maintain the limestone feeder at or above the level established during the most recent performance test; and</li> <li>d. Use the same grade of limestone from the same source as was used during the most recent performance test and maintain records of the source and type of limestone used.</li> </ul>
12. Each affected kiln that is equipped with a DIFF or DLS/FF	<ul style="list-style-type: none"> <li>a. Initiate corrective action within 1 hour of a bag leak detection system alarm and complete corrective actions in accordance with the OM&amp;M plan; and</li> <li>b. Verify at least once each 8-hour shift that lime is free-flowing by means of a visual check, checking the output of a load cell, carrier gas/lime flow indicator, or carrier gas pressure drop measurement system; and</li> <li>c. Record the lime feeder setting daily to verify that the feeder setting is at or above the level established during the most recent performance test.</li> </ul>
13. Each affected kiln that is equipped with a wet scrubber .....	<ul style="list-style-type: none"> <li>a. Maintain the 3-hour block average pressure drop across the scrubber, liquid pH, and liquid flow rate at or above the minimum levels established during the most recent performance test; and</li> <li>b. If chemicals are added to the scrubber liquid, maintain the 3-hour block average chemical feed rate at or above the minimum chemical feed rate established during the most recent performance test.</li> </ul>

TABLE 3 TO SUBPART SSSSS OF PART 63—WORK PRACTICE STANDARDS

As stated in §63.9788, you must comply with the work practice standards for affected sources in the following table:

For . . .	You must . . .	According to one of the following requirements . . .
1. Each basket or container that is used for holding fired refractory shapes in an existing shape preheater and autoclave during the pitch impregnation process.	a. Control POM emissions from any affected shape preheater.	i. At least every 10 preheating cycles, clean the residual pitch from the surfaces of the basket or container by abrasive blasting prior to placing the basket or container in the affected shape preheater; or ii. At least every 10 preheating cycles, subject the basket or container to a thermal process cycle that meets or exceeds the operating temperature and cycle time of the affected preheater, AND is conducted in a process unit that is exhausted to a thermal or catalytic oxidizer that is comparable to the control device used on an affected defumer or coking oven; or iii. Capture emissions from the affected shape preheater and vent them to the control device that is used to control emissions from an affected defumer or coking oven, or to a comparable thermal or catalytic oxidizer.
2. Each new or existing pitch working tank.	Control POM emissions .....	Capture emissions from the affected pitch working tank and vent them to the control device that is used to control emissions from an affected defumer or coking oven, OR to a comparable thermal or catalytic oxidizer.
3. Each new or existing chromium refractory products kiln.	Minimize fuel-based HAP emissions .....	Use natural gas, or equivalent, as the kiln fuel, except during periods of natural gas curtailment or supply interruption, as defined in §63.9824.
4. Each existing clay refractory products kiln.	Minimize fuel-based HAP emissions .....	Use natural gas, or equivalent, as the kiln fuel, except during periods of natural gas curtailment or supply interruption, as defined in §63.9824.

TABLE 4 TO SUBPART SSSSS TO PART 63—REQUIREMENTS FOR PERFORMANCE TESTS

As stated in §63.9800, you must comply with the requirements for performance tests for affected sources in the following table:

For . . .	You must . . .	Using . . .	According to the following requirements . . .
1. Each affected source listed in Table 1 to this subpart.	a. Conduct performance tests .....	i. The requirements of the general provisions in subpart A of this part and the requirements to this subpart.	(1) Record the date of the test; and (2) Identify the emission source that is tested; and (3) Collect and record the corresponding operating parameter and emission test data listed in this table for each run of the performance test; and (4) Repeat the performance test at least every 5 years; and (5) Repeat the performance test before changing the parameter value for any operating limit specified in your OM&M plan; and

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For . . .	You must . . .	Using . . .	According to the following require-ments . . .
	<p>b. Select the locations of sampling ports and the number of tra-verse points.</p> <p>c. Determine gas velocity and vol-umetric flow rate.</p> <p>d. Conduct gas molecular weight analysis.</p> <p>e. Measure gas moisture content</p>	<p>i. Method 1 or 1A of 40 CFR part 60, appendix A.</p> <p>Method 2, 2A, 2C, 2D, 2F, or 2G of 40 CFR part 60, appendix A.</p> <p>(i) Method 3, 3A, or 3B of 40 CFR part 60, appendix A; or</p> <p>(ii) ASME PTC 19.10–1981–Part 10.</p> <p>Method 4 of 40 CFR part 60, ap-pendix A.</p>	<p>(6) If complying with the THC con-centration or THC percentage reduction limits specified in items 2 through 9 of Table 1 to this subpart, repeat the perform-ance test under the conditions specified in items 2.a.2. and 2.a.3. of this table; and</p> <p>(7) If complying with the emission limits for new clay refractory products kilns specified in items 10 and 11 of Table 1 to this subpart, repeat the performance test under the conditions speci-fied in items 14.a.i.4. and 17.a.i.4. of this table.</p> <p>(1) To demonstrate compliance with the percentage reduction limits specified in items 2.b., 3.b., 6.b., 7.b., 10, and 11 of Table 1 to this subpart, locate sampling sites at the inlet of the control device and at either the outlet of the control device or at the stack prior to any releases to the atmosphere; and</p> <p>(2) To demonstrate compliance with any other emission limit specified in Table 1 to this sub-part, locate all sampling sites at the outlet of the control device or at the stack prior to any re-leases to the atmosphere.</p> <p>Measure gas velocities and volu-metric flow rates at 1-hour inter-vals throughout each test run.</p> <p>As specified in the applicable test method.</p> <p>You may use ASME PTC 19.10–1981–Part 10 (available for pur-chase from Three Park Avenue, New York, NY 10016–5990) as an alternative to EPA Method 3B.</p> <p>As specified in the applicable test method.</p>

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For . . .	You must . . .	Using . . .	According to the following require-ments . . .
<p>2. Each new or existing curing oven, shape dryer, and kiln that is used to process refractory products that use organic HAP; each new or existing coking oven and defumer that is used to produce pitch-impregnated refractory products; each new shape preheater that is used to produce pitch-impregnated refractory products; AND each new or existing process unit that is exhausted to a thermal or catalytic oxidizer that also controls emissions from an affected shape preheater or pitch working tank.</p>	<p>a. Conduct performance tests . . . . .</p> <p>b. Satisfy the applicable requirements listed in items 3 through 13 of this table.</p>	<p>.....</p>	<p>(1) Conduct the performance test while the source is operating at the maximum organic HAP processing rate, as defined in §63.9824, reasonably expected to occur; and</p> <p>(2) Repeat the performance test before starting production of any product for which the organic HAP processing rate is likely to exceed the maximum organic HAP processing rate established during the most recent performance test by more than 10 percent, as specified in §63.9798(c); and</p> <p>(3) Repeat the performance test on any affected uncontrolled kiln following process changes (e.g., shorter curing oven cycle time) that could increase organic HAP emissions from the affected kiln, as specified in §63.9798(d).</p>
<p>3. Each affected continuous process unit.</p>	<p>a. Perform a minimum of 3 test runs.</p> <p>b. Establish the operating limit for the maximum organic HAP processing rate.</p> <p>c. Record the operating temperature of the affected source.</p>	<p>The appropriate test methods specified in items 1, 4, and 5 of this table.</p> <p>i. Method 311 of 40 CFR part 63, appendix A, OR material safety data sheets (MSDS), OR product labels to determine the mass fraction of organic HAP in each resin, binder, or additive; and</p> <p>ii. Product formulation data that specify the mass fraction of each resin, binder, and additive in the products that are processed during the performance test; and</p> <p>iii. Process feed rate data (tons per hour).</p> <p>Process data .....</p>	<p>Each test run must be at least 1 hour in duration.</p> <p>(1) Calculate and record the organic HAP content of all refractory shapes that are processed during the performance test, based on the mass fraction of organic HAP in the resins, binders, or additives; the mass fraction of each resin, binder, or additive, in the product; and the process feed rate; and</p> <p>(2) Calculate and record the organic HAP processing rate (pounds per hour) for each test run; and</p> <p>(3) Calculate and record the maximum organic HAP processing rate as the average of the organic HAP processing rates for the three test runs.</p> <p>During each test run and at least once per hour, record the operating temperature in the highest temperature zone of the affected source.</p>

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For . . .	You must . . .	Using . . .	According to the following require-ments . . .
<p>4. Each continuous process unit that is subject to the THC emission limit listed in item 2.a., 3.a., 4, or 5 of Table 1 to this subpart.</p>	<p>a. Measure THC concentrations at the outlet of the control device or in the stack.</p> <p>b. Measure oxygen concentrations at the outlet of the control device or in the stack.</p> <p>c. Determine the hourly average THC concentration, corrected to 18 percent oxygen.</p> <p>d. Determine the 3-hour block average THC emission concentration, corrected to 18 percent oxygen.</p>	<p>i. Method 25A of 40 CFR part 60, appendix A.</p> <p>i. Method 3A of 40 CFR part 60, appendix A.</p> <p>i. Equation 1 of §63.9800(g)(1); and. ii. The 1-minute THC and oxygen concentration data.</p> <p>The hourly average concentration of THC, corrected to 18 percent oxygen, for each test run.</p>	<p>(1) Each minute, measure and record the concentrations of THC in the exhaust stream; and (2) Provide at least 50 1-minute measurements for each valid hourly average THC concentration.</p> <p>(1) Each minute, measure and record the concentrations of oxygen in the exhaust stream; and (2) Provide at least 50 1-minute measurements for each valid hourly average THC concentration.</p> <p>(1) Calculate the hourly average THC concentration for each hour of the performance test as the average of the 1-minute THC measurements; and (2) Calculate the hourly average oxygen concentration for each hour of the performance test as the average of the 1-minute oxygen measurements; and (3) Correct the hourly average THC concentrations to 18 percent oxygen using Equation 1 of §63.9800(g)(1).</p> <p>Calculate the 3-hour block average THC emission concentration, corrected to 18 percent oxygen, as the average of the hourly average THC emission concentrations, corrected to 18 percent oxygen.</p>
<p>5. Each continuous process unit that is subject to the THC percentage reduction limit listed in item 2.b. or 3.b. of Table 1 to this subpart.</p>	<p>a. Measure THC concentrations at the inlet and outlet of the control device.</p> <p>b. Determine the hourly THC mass emissions rates at the inlet and outlet of the control device.</p> <p>c. Determine the 3-hour block average THC percentage reduction.</p>	<p>i. Method 25A of 40 CFR part 60, appendix A.</p> <p>i. The 1-minute THC concentration data at the control device inlet and outlet; and ii. The volumetric flow rates at the control device inlet and outlet.</p> <p>i. The hourly THC mass emissions rates at the inlet and outlet of the control device.</p>	<p>(1) Each minute, measure and record the concentrations of THC at the inlet and outlet of the control device; and (2) Provide at least 50 1-minute measurements for each valid hourly average THC concentration at the control device inlet and outlet.</p> <p>Calculate the hourly THC mass emissions rates at the control device inlet and outlet for each hour of the performance test.</p> <p>(1) Calculate the hourly THC percentage reduction for each hour of the performance test using Equation 2 of §63.9800(g)(1); and (2) Calculate the 3-hour block average THC percentage reduction.</p>

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For . . .	You must . . .	Using . . .	According to the following requirements . . .
6. Each continuous process unit that is equipped with a thermal oxidizer.	a. Establish the operating limit for the minimum allowable thermal oxidizer combustion chamber temperature.	i. Continuous recording of the output of the combustion chamber temperature measurement device.	<ul style="list-style-type: none"> <li>(1) At least every 15 minutes, measure and record the thermal oxidizer combustion chamber temperature; and</li> <li>(2) Provide at least one measurement during at least three 15-minute periods per hour of testing; and</li> <li>(3) Calculate the hourly average thermal oxidizer combustion chamber temperature for each hour of the performance test; and</li> <li>(4) Calculate the minimum allowable combustion chamber temperature as the average of the combustion chamber temperatures for the three test runs, minus 14 °C (25 °F).</li> </ul>
7. Each continuous process unit that is equipped with a catalytic oxidizer.	a. Establish the operating limit for the minimum allowable temperature at the inlet of the catalyst bed.	i. Continuous recording of the output of the temperature measurement device.	<ul style="list-style-type: none"> <li>(1) At least every 15 minutes, measure and record the temperature at the inlet of the catalyst bed; and</li> <li>(2) Provide at least one catalyst bed inlet temperature measurement during at least three 15-minute periods per hour of testing; and</li> <li>(3) Calculate the hourly average catalyst bed inlet temperature for each hour of the performance test; and</li> <li>(4) Calculate the minimum allowable catalyst bed inlet temperature as the average of the catalyst bed inlet temperatures for the three test runs, minus 14 °C (25 °F).</li> </ul>
8. Each affected batch process unit.	a. Perform a minimum of two test runs.	i. The appropriate test methods specified in items 1, 9, and 10 of this table.	<ul style="list-style-type: none"> <li>(1) Each test run must be conducted over a separate batch cycle unless you satisfy the requirements of § 63.9800(f)(3) and (4); and</li> <li>(2) Each test run must begin with the start of a batch cycle, except as specified in item 8.a.i.4. of this table; and</li> <li>(3) Each test run must continue until the end of the batch cycle, except as specified in items 8.a.i.4. and 8.a.i.5. of this table; and</li> <li>(4) If you develop an emissions profile, as described in § 63.9802(a), AND for sources equipped with a thermal or catalytic oxidizer, you do not reduce the oxidizer operating temperature, as specified in item 13 of this table, you can limit each test run to the 3-hour peak THC emissions period; and</li> </ul>

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For . . .	You must . . .	Using . . .	According to the following requirements . . .
<p>9. Each batch process unit that is subject to the THC emission limit listed in item 6.a., 7.a., 8, or 9 of Table 1 to this subpart.</p>	<p>b. Establish the operating limit for the maximum organic HAP processing rate.</p> <p>c. Record the batch cycle time . . . .</p> <p>d. Record the operating temperature of the affected source.</p> <p>a. Measure THC concentrations at the outlet of the control device or in the stack.</p>	<p>i. Method 311 of 40 CFR part 63, appendix A, OR MSDS, OR product labels to determine the mass fraction of organic HAP in each resin, binder, or additive; and</p> <p>ii. Product formulation data that specify the mass fraction of each resin, binder, and additive in the products that are processed during the performance test; and</p> <p>iii. Batch weight (tons) . . . . .</p> <p>Process data . . . . .</p> <p>Process data . . . . .</p> <p>i. Method 25A of 40 CFR part 60, appendix A.</p>	<p>(5) If you do not develop an emissions profile, a test run can be stopped, and the results of that run considered complete, if you measure emissions continuously until at least 3 hours after the affected process unit has reached maximum temperature, AND the hourly average THC mass emissions rate has not increased during the 3-hour period since maximum process temperature was reached, and the hourly average concentrations of THC at the inlet of the control device have not exceeded 20 ppmvd, corrected to 18 percent oxygen, during the 3-hour period since maximum process temperature was reached or the hourly average THC percentage reduction has been at least 95 percent during the 3-hour period since maximum process temperature was reached, AND, for sources equipped with a thermal or catalytic oxidizer, at least 1 hour has passed since any reduction in the operating temperature of the oxidizer, as specified in item 13 of this table.</p> <p>(1) Calculate and record the organic HAP content of all refractory shapes that are processed during the performance test, based on the mass fraction of HAP in the resins, binders, or additives; the mass fraction of each resin, binder, or additive, in the product, and the batch weight prior to processing; and</p> <p>(2) Calculate and record the organic HAP processing rate (pounds per batch) for each test run; and</p> <p>(3) Calculate and record the maximum organic HAP processing rate as the average of the organic HAP processing rates for the two test runs.</p> <p>Record the total elapsed time from the start to the completion of the batch cycle.</p> <p>Record the operating temperature of the affected source at least once every hour from the start to the completion of the batch cycle.</p> <p>(1) Each minute, measure and record the concentrations of THC in the exhaust stream; and</p> <p>(2) Provide at least 50 1-minute measurements for each valid hourly average THC concentration.</p>

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For . . .	You must . . .	Using . . .	According to the following requirements . . .
10. Each batch process unit that is subject to the THC percentage reduction limit listed in item 6.b. or 7.b. of Table 1 to this subpart.	b. Measure oxygen concentrations at the outlet of the control device or in the stack.	i. Method 3A of 40 CFR part 60, appendix A.	(1) Each minute, measure and record the concentrations of oxygen in the exhaust stream; and (2) Provide at least 50 1-minute measurements for each valid hourly average oxygen concentration.
	c. Determine the hourly average THC concentration, corrected to 18 percent oxygen.	i. Equation 1 of §63.9800(g)(1); and ii. The 1-minute THC and oxygen concentration data.	(1) Calculate the hourly average THC concentration for each hour of the performance test as the average of the 1-minute THC measurements; and (2) Calculate the hourly average oxygen concentration for each hour of the performance test as the average of the 1-minute oxygen measurements; and (3) Correct the hourly average THC concentrations to 18 percent oxygen using Equation 1 of §63.9800(g)(1).
	d. Determine the 3-hour peak THC emissions period for each test run.	The hourly average THC concentrations, corrected to 18 percent oxygen.	Select the period of 3 consecutive hours over which the sum of the hourly average THC concentrations, corrected to 18 percent oxygen, is greater than the sum of the hourly average THC emission concentrations, corrected to 18 percent oxygen, for any other period of 3 consecutive hours during the test run.
	e. Determine the average THC concentration, corrected to 18 percent oxygen, for each test run.	The hourly average THC emission concentrations, corrected to 18 percent oxygen, for the 3-hour peak THC emissions period.	Calculate the average of the hourly average THC concentrations, corrected to 18 percent oxygen, for the 3 hours of the peak emissions period for each test run.
	f. Determine the 2-run block average THC concentration, corrected to 18 percent oxygen, for the emission test.	The average THC concentration, corrected to 18 percent oxygen, for each test run.	Calculate the average of the average THC concentrations, corrected to 18 percent oxygen, for each run.
	a. Measure THC concentrations at the inlet and outlet of the control device.	i. Method 25A of 40 CFR part 60, appendix A.	(1) Each minute, measure and record the concentrations of THC at the control device inlet and outlet; and (2) Provide at least 50 1-minute measurements for each valid hourly average THC concentration at the control device inlet and outlet.
	b. Determine the hourly THC mass emissions rates at the control device inlet and outlet.	i. The 1-minute THC concentration data at the control device inlet and outlet; and ii. The volumetric flow rates at the control device inlet and outlet.	(1) Calculate the hourly mass emissions rates at the control device inlet and outlet for each hour of the performance test.
	c. Determine the 3-hour peak THC emissions period for each test run.	The hourly THC mass emissions rates at the control device inlet.	Select the period of 3 consecutive hours over which the sum of the hourly THC mass emissions rates at the control device inlet is greater than the sum of the hourly THC mass emissions rates at the control device inlet for any other period of 3 consecutive hours during the test run.
	d. Determine the average THC percentage reduction for each test run.	i. Equation 2 of §63.9800(g)(2); and ii. The hourly THC mass emissions rates at the control device inlet and outlet for the 3-hour peak THC emissions period.	Calculate the average THC percentage reduction for each test run using Equation 2 of §63.9800(g)(2).

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For . . .	You must . . .	Using . . .	According to the following requirements . . .
11. Each batch process unit that is equipped with a thermal oxidizer.	<ul style="list-style-type: none"> <li>e. Determine the 2-run block average THC percentage reduction for the emission test.</li> <li>a. Establish the operating limit for the minimum thermal oxidizer combustion chamber temperature.</li> </ul>	<ul style="list-style-type: none"> <li>The average THC percentage reduction for each test run.</li> <li>i. Continuous recording of the output of the combustion chamber temperature measurement device.</li> </ul>	<p>Calculate the average of the average THC percentage reductions for each test run.</p> <ul style="list-style-type: none"> <li>(1) At least every 15 minutes, measure and record the thermal oxidizer combustion chamber temperature; and</li> <li>(2) Provide at least one temperature measurement during at least three 15-minute periods per hour of testing; and</li> <li>(3) Calculate the hourly average combustion chamber temperature for each hour of the 3-hour peak emissions period, as defined in item 9.d. or 10.c. of this table, whichever applies; and</li> <li>(4) Calculate the minimum allowable thermal oxidizer combustion chamber operating temperature as the average of the hourly combustion chamber temperatures for the 3-hour peak emissions period, minus 14 °C (25 °F).</li> </ul>
12. Each batch process unit that is equipped with a catalytic oxidizer.	<ul style="list-style-type: none"> <li>a. Establish the operating limit for the minimum temperature at the inlet of the catalyst bed.</li> </ul>	<ul style="list-style-type: none"> <li>i. Continuous recording of the output of the temperature measurement device.</li> </ul>	<ul style="list-style-type: none"> <li>(1) At least every 15 minutes, measure and record the temperature at the inlet of the catalyst bed; and</li> <li>(2) Provide at least one catalyst bed inlet temperature measurement during at least three 15-minute periods per hour of testing; and</li> <li>(3) Calculate the hourly average catalyst bed inlet temperature for each hour of the 3-hour peak emissions period, as defined in item 9.d. or 10.c. of this table, whichever applies; and</li> <li>(4) Calculate the minimum allowable catalytic oxidizer catalyst bed inlet temperature as the average of the hourly catalyst bed inlet temperatures for the 3-hour peak emissions period, minus 14 °C (25 °F).</li> </ul>
13. Each batch process unit that is equipped with a thermal or catalytic oxidizer.	<ul style="list-style-type: none"> <li>a. During each test run, maintain the applicable operating temperature of the oxidizer until emission levels allow the oxidizer to be shut off or the operating temperature of the oxidizer to be reduced.</li> </ul>		<ul style="list-style-type: none"> <li>(1) The oxidizer can be shut off or the oxidizer operating temperature can be reduced if you do not use an emission profile to limit testing to the 3-hour peak emissions period, as specified in item 8.a.i.4. of this table; and</li> <li>(2) At least 3 hours have passed since the affected process unit reached maximum temperature; and</li> <li>(3) The applicable emission limit specified in item 6.a. or 6.b. of Table 1 to this subpart was met during each of the previous three 1-hour periods; and</li> <li>(4) The hourly average THC mass emissions rate did not increase during the 3-hour period since maximum process temperature was reached; and</li> </ul>

For . . .	You must . . .	Using . . .	According to the following require-ments . . .
<p>14. Each new continuous kiln that is used to process clay refractory products.</p>	<p>a. Measure emissions of HF and HCl.</p>	<p>i. Method 26A of 40 CFR part 60, appendix A; or                      ii. Method 26 of 40 CFR part 60, appendix A; or                      iii. Method 320 of 40 CFR part 63, appendix A.</p>	<p>(5) The applicable emission limit specified in item 6.a. and 6.b. of Table 1 to this subpart was met during each of the four 15-minute periods immediately following the oxidizer temperature reduction; and                      (6) If the applicable emission limit specified in item 6.a. or 6.b. of Table 1 to this subpart was not met during any of the four 15-minute periods immediately following the oxidizer temperature reduction, you must return the oxidizer to its normal operating temperature as soon as possible and maintain that temperature for at least 1 hour; and                      (7) Continue the test run until the applicable emission limit specified in items 6.a. and 6.b. of Table 1 to this subpart is met for at least four consecutive 15-minute periods that immediately follow the temperature reduction; and                      (8) Calculate the hourly average oxidizer operating temperature for each hour of the performance test since the affected process unit reached maximum temperature.</p>
<p>15. Each new continuous kiln that is subject to the production-based HF and HCl emission limits specified in items 10.a. and 10.b. of Table 1 to this subpart.</p>	<p>b. Perform a minimum of 3 test runs.                       a. Record the uncalcined clay processing rate.</p>	<p>The appropriate test methods specified in items 1 and 14.a. of this table.                       i. Production data; and .....                      ii. Product formulation data that specify the mass fraction of uncalcined clay in the products that are processed during the performance test.</p>	<p>(1) Conduct the test while the kiln is operating at the maximum production level; and                      (2) You may use Method 26 of 40 CFR part 60, appendix A, only if no acid PM (e.g., HF or HCl dissolved in water droplets emitted by sources controlled by a wet scrubber) is present; and                      (3) If you use Method 320 of 40 CFR part 63, appendix A, you must follow the analyte spiking procedures of Section 13 of Method 320 unless you can demonstrate that the complete spiking procedure has been conducted at a similar source; and                      (4) Repeat the performance test if the affected source is controlled with a DLA and you change the source of the limestone used in the DLA.                       Each test run must be at least 1 hour in duration.</p>
			<p>(1) Record the production rate (tons per hour of fired product); and                      (2) Calculate and record the average rate at which uncalcined clay is processed (tons per hour) for each test run; and                      (3) Calculate and record the 3-run average uncalcined clay processing rate as the average of the average uncalcined clay processing rates for each test run.</p>

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For . . .	You must . . .	Using . . .	According to the following requirements . . .
<p>16. Each new continuous kiln that is subject to the HF and HCl percentage reduction limits specified in items 10.a. and 10.b. of Table 1 to this subpart.</p>	<p>b. Determine the HF mass emissions rate at the outlet of the control device or in the stack.</p>	<p>i. Method 26A of 40 CFR part 60, appendix A; or                      ii. Method 26 of 40 CFR part 60, appendix A; or                      iii. Method 320 of 40 CFR part 63, appendix A.</p>	<p>Calculate the HF mass emissions rate for each test.</p>
	<p>c. Determine the 3-hour block average production-based HF emissions rate.</p>	<p>i. The HF mass emissions rate for each test run; and                      ii. The average uncalcined clay processing rate.</p>	<p>(1) Calculate the hourly production-based HF emissions rate for each test run using Equation 3 of § 63.9800(g)(3); and                      (2) Calculate the 3-hour block average production-based HF emissions rate as the average of the hourly production-based HF emissions rates for each test run.</p>
	<p>d. Determine the HCl mass emissions rate at the outlet of the control device or in the stack.</p>	<p>i. Method 26A of 40 CFR part 60, appendix A; or                      ii. Method 26 of 40 CFR part 60, appendix A; or                      iii. Method 320 of 40 CFR part 63, appendix A.</p>	<p>Calculate the HCl mass emissions rate for each test run.</p>
	<p>e. Determine the 3-hour block average production-based HCl emissions rate.</p>	<p>i. The HCl mass emissions rate for each test run; and                      ii. The average uncalcined clay processing rate.</p>	<p>(1) Calculate the hourly production-based HCl emissions rate for each test run using Equation 3 of § 63.9800(g)(3); and                      (2) Calculate the 3-hour block average production-based HCl emissions rate as the average of the production-based HCl emissions rates for each test run.</p>
	<p>a. Measure the HF mass emissions rates at the inlet and outlet of the control device.</p>	<p>i. Method 26A of 40 CFR part 60, appendix A; or                      ii. Method 26 of 40 CFR part 60, appendix A; or                      iii. Method 320 of 40 CFR part 63, appendix A.</p>	<p>Calculate the HF mass emissions rates at the control device inlet and outlet for each test run.</p>
	<p>b. Determine the 3-hour block average HF percentage reduction.</p>	<p>i. The HF mass emissions rates at the inlet and outlet of the control device for each test run</p>	<p>(1) Calculate the hourly HF percentage reduction using Equation 2 of § 63.9800(g)(2); and                      (2) Calculate the 3-hour block average HF percentage reduction as the average of the HF percentage reductions for each test run.</p>
	<p>c. Measure the HCl mass emissions rates at the inlet and outlet of the control device.</p>	<p>i. Method 26A of 40 CFR part 60, appendix A; or                      ii. Method 26 of 40 CFR part 60, appendix A; or                      iii. Method 320 of 40 CFR part 63, appendix A.</p>	<p>Calculate the HCl mass emissions rates at the control device inlet and outlet for each test run.</p>
	<p>d. Determine the 3-hour block average HCl percentage reduction.</p>	<p>i. The HCl mass emissions rates at the inlet and outlet of the control device for each test run.</p>	<p>(1) Calculate the hourly HCl percentage reduction using Equation 2 of § 63.9800(g)(2); and                      (2) Calculate the 3-hour block average HCl percentage reduction as the average of HCl percentage reductions for each test run.</p>

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For . . .	You must . . .	Using . . .	According to the following requirements . . .
17. Each new batch process kiln that is used to process clay refractory products.	<p>a. Measure emissions of HF and HCl at the inlet and outlet of the control device.</p> <p>b. Perform a minimum of 2 test runs.</p> <p>c. Determine the hourly HF and HCl mass emissions rates at the inlet and outlet of the control device.</p> <p>d. Determine the 3-hour peak HF emissions period.</p> <p>e. Determine the 2-run block average HF percentage reduction for the emissions test.</p>	<p>i. Method 26A of 40 CFR part 60, appendix A; or</p> <p>ii. Method 26 of 40 CFR part 60, appendix A; or</p> <p>iii. Method 320 of 40 CFR part 63, appendix A.</p> <p>i. The appropriate test methods specified in items 1 and 17.a. of this table.</p> <p>i. The appropriate test methods specified in items 1 and 17.a. of this table.</p> <p>The hourly HF mass emissions rates at the inlet of the control device.</p> <p>i. The hourly average HF emissions rates at the inlet and outlet of the control device.</p>	<p>(1) Conduct the test while the kiln is operating at the maximum production level; and</p> <p>(2) You may use Method 26 of 40 CFR part 60, appendix A, only if no acid PM (e.g., HF or HCl dissolved in water droplets emitted by sources controlled by a wet scrubber) is present; and</p> <p>(3) If you use Method 320 of 40 CFR part 63, you must follow the analyte spiking procedures of Section 13 of Method 320 unless you can demonstrate that the complete spiking procedure has been conducted at a similar source; and</p> <p>(4) Repeat the performance test if the affected source is controlled with a DLA and you change the source of the limestone used in the DLA.</p> <p>(1) Each test run must be conducted over a separate batch cycle unless you satisfy the requirements of § 63.9800(f)(3) and (4); and</p> <p>(2) Each test run must consist of a series of 1-hour runs at the inlet and outlet of the control device, beginning with the start of a batch cycle, except as specified in item 17.b.i.4. of this table; and</p> <p>(3) Each test run must continue until the end of the batch cycle, except as specified in item 17.b.i.4. of this table; and</p> <p>(4) If you develop an emissions profile, as described in § 63.9802(b), you can limit each test run to the 3-hour peak HF emissions period.</p> <p>Determine the hourly mass HF and HCl emissions rates at the inlet and outlet of the control device for each hour of each test run.</p> <p>Select the period of 3 consecutive hours over which the sum of the hourly HF mass emissions rates at the control device inlet is greater than the sum of the hourly HF mass emissions rates at the control device inlet for any other period of 3 consecutive hours during the test run.</p> <p>(1) Calculate the HF percentage reduction for each hour of the 3-hour peak HF emissions period using Equation 2 of § 63.9800(g)(2); and</p> <p>(2) Calculate the average HF percentage reduction for each test run as the average of the hourly HF percentage reductions for the 3-hour peak HF emissions period for that run; and</p>

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For . . .	You must . . .	Using . . .	According to the following requirements . . .
<p>18. Each new kiln that is used to process clay refractory products and is equipped with a DLA.</p>	<p>f. Determine the 2-run block average HCl percentage reduction for the emission test.</p> <p>a. Establish the operating limit for the minimum pressure drop across the DLA.</p> <p>b. Establish the operating limit for the limestone feeder setting.</p>	<p>i. The hourly average HCl emissions rates at the inlet and outlet of the control device.</p> <p>Data from the pressure drop measurement device during the performance test.</p> <p>Data from the limestone feeder during the performance test.</p>	<p>(3) Calculate the 2-run block average HF percentage reduction for the emission test as the average of the average HF percentage reductions for the two test runs.</p> <p>(1) Calculate the HCl percentage reduction for each hour of the 3-hour peak HF emissions period using Equation 2 §63.9800(g)(2); and</p> <p>(2) Calculate the average HCl percentage reduction for each test run as the average of the hourly HCl percentage reductions for the 3-hour peak HF emissions period for that run; and</p> <p>(3) Calculate the 2-run block average HCl percentage reduction for the emission test as the average of the average HCl percentage reductions for the two test runs.</p> <p>(1) At least every 15 minutes, measure the pressure drop across the DLA; and</p> <p>(2) Provide at least one pressure drop measurement during at least three 15-minute periods per hour of testing; and</p> <p>(3) Calculate the hourly average pressure drop across the DLA for each hour of the performance test; and</p> <p>(4) Calculate and record the minimum pressure drop as the average of the hourly average pressure drops across the DLA for the two or three test runs, whichever applies.</p> <p>(1) Ensure that limestone in the feed hopper, silo, and DLA is free-flowing at all times during the performance test; and</p> <p>(2) Establish the limestone feeder setting 1 week prior to the performance test; and</p> <p>(3) Record and maintain the feeder setting for the 1-week period that precedes the performance test and during the performance test.</p>
<p>19. Each new kiln that is used to process clay refractory products and is equipped with a DIFF or DLS/FF.</p>	<p>a. Document conformance with specifications and requirements of the bag leak detection system.</p> <p>b. Establish the operating limit for the lime feeder setting.</p>	<p>Data from the installation and calibration of the bag leak detection system.</p> <p>i. Data from the lime feeder during the performance test.</p>	<p>Submit analyses and supporting documentation demonstrating conformance with EPA guidance and specifications for bag leak detection systems as part of the Notification of Compliance Status.</p> <p>(1) For continuous lime injection systems, ensure that lime in the feed hopper or silo is free-flowing at all times during the performance test; and</p> <p>(2) Record the feeder setting for the three test runs; and</p> <p>(3) If the feed rate setting varies during the three test runs, calculate and record the average feed rate for the two or three test runs, whichever applies.</p>

For . . .	You must . . .	Using . . .	According to the following requirements . . .
<p>20. Each new kiln that is used to process clay refractory products and is equipped with a wet scrubber.</p>	<p>a. Establish the operating limit for the minimum scrubber pressure drop.</p>	<p>i. Data from the pressure drop measurement device during the performance test.</p>	<p>(1) At least every 15 minutes, measure the pressure drop across the scrubber; and                      (2) Provide at least one pressure drop measurement during at least three 15-minute periods per hour of testing; and                      (3) Calculate the hourly average pressure drop across the scrubber for each hour of the performance test; and                      (4) Calculate and record the minimum pressure drop as the average of the hourly average pressure drops across the scrubber for the two or three test runs, whichever applies.</p>
	<p>b. Establish the operating limit for the minimum scrubber liquid pH.</p>	<p>i. Data from the pH measurement device during the performance test.</p>	<p>(1) At least every 15 minutes, measure scrubber liquid pH; and                      (2) Provide at least one pH measurement during at least three 15-minute periods per hour of testing; and                      (3) Calculate the hourly average pH values for each hour of the performance test; and                      (4) Calculate and record the minimum liquid pH as the average of the hourly average pH measurements for the two or three test runs, whichever applies.</p>
	<p>c. Establish the operating limit for the minimum scrubber liquid flow rate.</p>	<p>i. Data from the flow rate measurement device during the performance test.</p>	<p>(1) At least every 15 minutes, measure the scrubber liquid flow rate; and                      (2) Provide at least one flow rate measurement during at least three 15-minute periods per hour of testing; and                      (3) Calculate the hourly average liquid flow rate for each hour of the performance test; and                      (4) Calculate and record the minimum liquid flow rate as the average of the hourly average liquid flow rates for the two or three test runs, whichever applies.</p>
	<p>d. If chemicals are added to the scrubber liquid, establish the operating limit for the minimum scrubber chemical feed rate.</p>	<p>i. Data from the chemical feed rate measurement device during the performance test.</p>	<p>(1) At least every 15 minutes, measure the scrubber chemical feed rate; and                      (2) Provide at least one chemical feed rate measurement during at least three 15-minute periods per hour of testing; and                      (3) Calculate the hourly average chemical feed rate for each hour of the performance test; and                      (4) Calculate and record the minimum chemical feed rate as the average of the hourly average chemical feed rates for the two or three test runs, whichever applies.</p>

TABLE 5 TO SUBPART SSSSS OF PART 63—INITIAL COMPLIANCE WITH EMISSION LIMITS

As stated in §63.9806, you must show initial compliance with the emission limits for affected sources according to the following table:

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For . . .	For the following emission limit . . .	You have demonstrated compliance if . . .
1. Each affected source listed in Table 1 to this subpart.	a. Each applicable emission limit listed in Table 1 to this subpart.	i. Emissions measured using the test methods specified in Table 4 to this subpart satisfy the applicable emission limits specified in Table 1 to this subpart; and ii. You establish and have a record of the operating limits listed in Table 2 to this subpart over the performance test period; and iii. You report the results of the performance test in the Notification of Compliance Status, as specified by §63.9812(e)(1) and (2).
2. Each new or existing curing oven, shape dryer, and kiln that is used to process refractory products that use organic HAP; each new or existing coking oven and defumer that is used to produce pitch-impregnated refractory products; each new shape preheater that is used to produce pitch-impregnated refractory products; AND each new or existing process unit that is exhausted to a thermal or catalytic oxidizer that also controls emissions from an affected shape preheater or pitch working tank.	As specified in items 3 through 8 of this table.	You have satisfied the applicable requirements specified in items 3 through 8 of this table.
3. Each affected continuous process unit that is subject to the THC emission concentration limit listed in item 2.a., 3.a., 4, or 5 of Table 1 to this subpart.	The average THC concentration must not exceed 20 ppmvd, corrected to 18 percent oxygen.	The 3-hour block average THC emission concentration measured during the performance test using Methods 25A and 3A is equal to or less than 20 ppmvd, corrected to 18 percent oxygen.
4. Each affected continuous process unit that is subject to the THC percentage reduction limit listed in item 2.b. or 3.b. of Table 1 to this subpart.	The average THC percentage reduction must equal or exceed 95 percent.	The 3-hour block average THC percentage reduction measured during the performance test using Method 25A is equal to or greater than 95 percent.
5. Each affected batch process unit that is subject to the THC emission concentration limit listed in item 6.a., 7.a., 8, or 9 of Table 1 to this subpart.	The average THC concentration must not exceed 20 ppmvd, corrected to 18 percent oxygen.	The 2-run block average THC emission concentration for the 3-hour peak emissions period measured during the performance test using Methods 25A and 3A is equal to or less than 20 ppmvd, corrected to 18 percent oxygen.
6. Each affected batch process unit that is subject to the THC percentage reduction limit listed in item 6.b. or 7.b. of Table 1 to this subpart.	The average THC percentage reduction must equal or exceed 95 percent.	The 2-run block average THC percentage reduction for the 3-hour peak emissions period measured during the performance test using Method 25A is equal to or exceeds 95 percent.
7. Each affected continuous or batch process unit that is equipped with a control device other than a thermal or catalytic oxidizer and is subject to the emission limit listed in item 3 or 7 of Table 1 to this subpart.	a. The average THC concentration must not exceed 20 ppmvd, corrected to 18 percent oxygen; or  b. The average THC percentage reduction must equal or exceed 95 percent.	i. You have installed a THC CEMS at the outlet of the control device or in the stack of the affected source; and  ii. You have satisfied the requirements of PS-8 of 40 CFR part 60, appendix B.
8. Each affected continuous or batch process unit that uses process changes to reduce organic HAP emissions and is subject to the emission limit listed in item 4 or 8 of Table 1 to this subpart.	The average THC concentration must not exceed 20 ppmvd, corrected to 18 percent oxygen.	i. You have installed a THC CEMS at the outlet of the control device or in the stack of the affected source; and ii. You have satisfied the requirements of PS-8 of 40 CFR part 60, appendix B.
9. Each new continuous kiln that is used to process clay refractory products.	a. The average HF emissions must not exceed 0.019 kg/Mg (0.038 lb/ton) of uncalcined clay processed; OR the average uncontrolled HF emissions must be reduced by at least 90 percent.	i. The 3-hour block average production-based HF emissions rate measured during the performance test using one of the methods specified in item 14.a.i. of Table 4 to this subpart is equal to or less than 0.019 kg/Mg (0.038 lb/ton) of uncalcined clay processed; or ii. The 3-hour block average HF emissions reduction measured during the performance test is equal to or greater than 90 percent.

For . . .	For the following emission limit . . .	You have demonstrated compliance if . . .
10. Each new batch process kiln that is used to process clay refractory products.	<p>b. The average HCl emissions must not exceed 0.091 kg/Mg (0.18 lb/ton) of uncalcined clay processed; OR the average uncontrolled HCl emissions must be reduced by at least 30 percent.</p> <p>a. The average uncontrolled HF emissions must be reduced by at least 90 percent.</p> <p>b. The average uncontrolled HCl emissions must be reduced by at least 30 percent.</p>	<p>i. The 3-hour block average production-based HCl emissions rate measured during the performance test using one of the methods specified in item 14.a.i. of Table 4 to this subpart is equal to or less than 0.091 kg/Mg (0.18 lb/ton) of uncalcined clay processed; or</p> <p>ii. The 3-hour block average HCl emissions reduction measured during the performance test is equal to or greater than 30 percent.</p> <p>The 2-run block average HF emission reduction measured during the performance test is equal to or greater than 90 percent.</p> <p>The 2-run block average HCl emissions reduction measured during the performance test is equal to or greater than 30 percent.</p>

TABLE 6 TO SUBPART SSSSS OF PART 63—INITIAL COMPLIANCE WITH WORK PRACTICE STANDARDS

As stated in §63.9806, you must show initial compliance with the work practice standards for affected sources according to the following table:

For each . . .	For the following standard . . .	You have demonstrated initial compliance if . . .
1. Each affected source listed in Table 3 to this subpart.	a. Each applicable work practice standard listed in Table 3 to this subpart.	<p>i. You have selected a method for performing each of the applicable work practice standards listed in Table 3 to this subpart; and</p> <p>ii. You have included in your Initial Notification a description of the method selected for complying with each applicable work practice standard, as required by §63.9(b); and</p> <p>iii. You submit a signed statement with the Notification of Compliance Status that you have implemented the applicable work practice standard listed in Table 3 to this subpart; and</p> <p>iv. You have described in your OM&amp;M plan the method for complying with each applicable work practice standard specified in Table 3 to this subpart.</p>
2. Each basket or container that is used for holding fired refractory shapes in an existing shape preheater and autoclave during the pitch impregnation process.	a. Control POM emissions from any affected shape preheater.	<p>i. You have implemented at least one of the work practice standards listed in item 1 of Table 3 to this subpart; and</p> <p>ii. You have established a system for recording the date and cleaning method for each time you clean an affected basket or container.</p>
3. Each affected new or existing pitch working tank.	Control POM emissions .....	You have captured and vented emissions from the affected pitch working tank to the device that is used to control emissions from an affected defumer or coking oven, or to a thermal or catalytic oxidizer that is comparable to the control device used on an affected defumer or coking oven.
4. Each new or existing chromium refractory products kiln.	Minimize fuel-based HAP emissions .....	You use natural gas, or equivalent, as the kiln fuel.
5. Each existing clay refractory products kiln.	Minimize fuel-based HAP emissions .....	You use natural gas, or equivalent, as the kiln fuel.

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**TABLE 7 TO SUBPART SSSSS OF PART 63—CONTINUOUS COMPLIANCE WITH EMISSION LIMITS**

As stated in §63.9810, you must show continuous compliance with the emission limits for affected sources according to the following table:

For . . .	For the following emission limit . . .	You must demonstrate continuous compliance by . . .
1. Each affected source listed in Table 1 to this subpart.	a. Each applicable emission limit listed in Table 1 to this subpart.	i. Collecting and recording the monitoring and process data listed in Table 2 (operating limits) to this subpart; and ii. Reducing the monitoring and process data associated with the operating limits specified in Table 2 to this subpart; and iii. Recording the results of any control device inspections; and iv. Reporting, in accordance with §63.9814(e), any deviation from the applicable operating limits specified in Table 2 to this subpart.
2. Each new or existing curing oven, shape dryer, and kiln that is used to process refractory products that use organic HAP; each new or existing coking oven and defumer that is used to produce pitch-impregnated refractory products; each new shape preheater that is used to produce pitch-impregnated refractory products; AND each new or existing process unit that is exhausted to a thermal or catalytic oxidizer that also controls emissions from an affected shape preheater or pitch working tank.	As specified in items 3 through 7 of this table.	Satisfying the applicable requirements specified in items 3 through 7 of this table.
3. Each affected process unit that is equipped with a thermal or catalytic oxidizer.	a. The average THC concentration must not exceed 20 ppmvd, corrected to 18 percent oxygen; OR the average THC percentage reduction must equal or exceed 95 percent.	i. Collecting the applicable data measured by the control device temperature monitoring system, as specified in items 5, 6, 8, and 9 of Table 8 to this subpart; and ii. Reducing the applicable data measured by the control device temperature monitoring system, as specified in items 5, 6, 8, and 9 of Table 8 to this subpart; and iii. Maintaining the average control device operating temperature for the applicable averaging period specified in items 5, 6, 8, and 9 of Table 2 to this subpart at or above the minimum allowable operating temperature established during the most recent performance test.
4. Each affected process unit that is equipped with a control device other than a thermal or catalytic oxidizer.	The average THC concentration must not exceed 20 ppmvd, corrected to 18 percent oxygen; OR the average THC performance reduction must equal or exceed 95 percent.	Operating and maintaining a THC CEMS at the outlet of the control device or in the stack of the affected source, according to the requirements of Procedure 1 of 40 CFR part 60, appendix F.
5. Each affected process unit that uses process changes to meet the applicable emission limit.	The average THC concentration must not exceed 20 ppmvd, corrected to 18 percent oxygen.	Operating and maintaining a THC CEMS at the outlet of the control device or in the stack of the affected source, according to the requirements of Procedure 1 of 40 CFR part 60, appendix F.
6. Each affected continuous process unit	The average THC concentration must not exceed 20 ppmvd, corrected to 18 percent oxygen; OR the average THC percentage reduction must equal or exceed 95 percent.	Recording the organic HAP processing rate (pounds per hour) and the operating temperature of the affected source, as specified in items 3.b. and 3.c. of Table 4 to this subpart.

For . . .	For the following emission limit . . .	You must demonstrate continuous compliance by . . .
7. Each affected batch process unit .....	The average THC concentration must not exceed 20 ppmvd, corrected to 18 percent oxygen; OR the average THC percentage reduction must equal or exceed 95 percent.	Recording the organic HAP processing rate (pounds per batch); and process cycle time for each batch cycle; and hourly average operating temperature of the affected source, as specified in items 8.b. through 8.d. of Table 4 to this subpart.
8. Each kiln that is used to process clay refractory products.	As specified in items 9 through 11 of this table.	Satisfying the applicable requirements specified in items 9 through 11 of this table.
9. Each affected kiln that is equipped with a DLA.	<p>a. The average HF emissions must not exceed 0.019 kg/Mg (0.038 lb/ton) of uncalcined clay processed, OR the average uncontrolled HF emissions must be reduced by at least 90 percent; and</p> <p>b. The average HCl emissions must not exceed 0.091 kg/Mg (0.18 lb/ton) of uncalcined clay processed, or the average uncontrolled HCl emissions must be reduced by at least 30 percent.</p>	<p>i. Maintaining the pressure drop across the DLA at or above the minimum levels established during the most recent performance test; and</p> <p>ii. Verifying that the limestone hopper contains an adequate amount of free-flowing limestone by performing a daily visual check of the limestone in the feed hopper; and</p> <p>iii. Recording the limestone feeder setting daily to verify that the feeder setting is at or above the level established during the most recent performance test; and</p> <p>iv. Using the same grade of limestone as was used during the most recent performance test and maintaining records of the source and grade of limestone.</p>
10. Each affected kiln that is equipped with a DIFF or DLS/FF.	<p>a. The average HF emissions must not exceed 0.019 kg/Mg (0.038 lb/ton) of uncalcined clay processed; OR the average uncontrolled HF emissions must be reduced by at least 90 percent; and</p> <p>b. The average HCl emissions must not exceed 0.091 kg/Mg (0.18 lb/ton) of uncalcined clay processed; OR the average uncontrolled HCl emissions must be reduced by at least 30 percent.</p>	<p>i. Verifying at least once each 8-hour shift that lime is free-flowing by means of a visual check, checking the output of a load cell, carrier gas/lime flow indicator, or carrier gas pressure drop measurement system; and</p> <p>ii. Recording feeder setting daily to verify that the feeder setting is at or above the level established during the most recent performance test; and</p> <p>iii. Initiating corrective action within 1 hour of a bag leak detection system alarm AND completing corrective actions in accordance with the OM&amp;M plan, AND operating and maintaining the fabric filter such that the alarm does not engage for more than 5 percent of the total operating time in a 6-month block reporting period.</p>
11. Each affected kiln that is equipped with a wet scrubber.	<p>a. The average HF emissions must not exceed 0.019 kg/Mg (0.038 lb/ton) of uncalcined clay processed; OR the average uncontrolled HF emissions must be reduced by at least 90 percent; and</p> <p>b. The average HCl emissions must not exceed 0.091 kg/Mg (0.18 lb/ton) of uncalcined clay processed; OR the average uncontrolled HCl emissions must be reduced by at least 30 percent.</p>	<p>i. Maintaining the pressure drop across the scrubber, liquid pH, and liquid flow rate at or above the minimum levels established during the most recent performance test; and</p> <p>ii. If chemicals are added to the scrubber liquid, maintaining the average chemical feed rate at or above the minimum chemical feed rate established during the most recent performance test.</p>

TABLE 8 TO SUBPART SSSSS OF PART 63—CONTINUOUS COMPLIANCE WITH OPERATING LIMITS

As stated in §63.9810, you must show continuous compliance with the operating limits for affected sources according to the following table:

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For . . .	For the following operating limit . . .	You must demonstrate continuous compliance by . . .
1. Each affected source listed in Table 2 to this subpart.	a. Each applicable operating limit listed in Table 2 to this subpart.	i. Maintaining all applicable process and control device operating parameters within the limits established during the most recent performance test; and
2. Each affected continuous kiln that is equipped with a control device.	a. The operating limits specified in items 2.a. through 2.c. of Table 2 to this subpart.	ii. Conducting annually an inspection of all duct work, vents, and capture devices to verify that no leaks exist and that the capture device is operating such that all emissions are properly vented to the control device in accordance with the OM&M plan.
3. Each new or existing curing oven, shape dryer, and kiln that is used to process refractory products that use organic HAP; each new or existing coking oven and defumer that is used to produce pitch-impregnated refractory products; each new shape preheater that is used to produce pitch-impregnated refractory products; AND each new or existing process unit that is exhausted to a thermal or catalytic oxidizer that also controls emissions from an affected shape preheater or pitch working tank.	As specified in items 4 through 9 of this table.	i. Operating the control device on the affected kiln during all times except during periods of approved scheduled maintenance, as specified in §63.9792(e); and ii. Minimizing HAP emissions from the affected kiln during all periods of scheduled maintenance of the kiln control device when the kiln is operating and the control device is out of service; and iii. Minimizing the duration of all periods of scheduled maintenance of the kiln control device when the kiln is operating and the control device is out of service.
4. Each affected continuous process unit	Maintain process operating parameters within the limits established during the most recent performance test.	Satisfying the applicable requirements specified in items 4 through 9 of this table.
5. Continuous process units that are equipped with a thermal oxidizer.	Maintain the 3-hour block average operating temperature in the thermal oxidizer combustion chamber at or above the minimum allowable operating temperature established during the most recent performance test.	i. Recording the organic HAP processing rate (pounds per hour); and ii. Recording the operating temperature of the affected source at least hourly; and iii. Maintaining the 3-hour block average organic HAP processing rate at or below the maximum organic HAP processing rate established during the most recent performance test.
		i. Measuring and recording the thermal oxidizer combustion chamber temperature at least every 15 minutes; and ii. Calculating the hourly average thermal oxidizer combustion chamber temperature; and iii. Maintaining the 3-hour block average thermal oxidizer combustion chamber temperature at or above the minimum allowable operating temperature established during the most recent performance test; and iv. Reporting, in accordance with §63.9814(e), any 3-hour block average operating temperature measurements below the minimum allowable thermal oxidizer combustion chamber operating temperature established during the most recent performance test.

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For . . .	For the following operating limit . . .	You must demonstrate continuous compliance by . . .
<p>6. Continuous process units that are equipped with a catalytic oxidizer.</p>	<p>a. Maintain the 3-hour block average temperature at the inlet of the catalyst bed at or above the minimum allowable catalyst bed inlet temperature established during the most recent performance test.</p>	<p>i. Measuring and recording the temperature at the inlet of the catalyst bed at least every 15 minutes; and                      ii. Calculating the hourly average temperature at the inlet of the catalyst bed; and                      iii. Maintaining the 3-hour block average temperature at the inlet of the catalyst bed at or above the minimum allowable catalyst bed inlet temperature established during the most recent performance test; and                      iv. Reporting, in accordance with §63.9814(e), any 3-hour block average catalyst bed inlet temperature measurements below the minimum allowable catalyst bed inlet temperature established during the most recent performance; and                      v. Checking the activity level of the catalyst at least every 12 months and taking any necessary corrective action, such as replacing the catalyst, to ensure that the catalyst is performing as designed.</p>
<p>7. Each affected batch process unit .....</p>	<p>Maintain process operating parameters within the limits established during the most recent performance test.</p>	<p>i. Recording the organic HAP processing rate (pounds per batch); and                      ii. Recording the hourly average operating temperature of the affected source; and                      iii. Recording the process cycle time for each batch cycle; and                      iv. Maintaining the organic HAP processing rate at or below the maximum organic HAP processing rate established during the most recent performance test.</p>
<p>8. Batch process units that are equipped with a thermal oxidizer.</p>	<p>Maintain the hourly average temperature in the thermal oxidizer combustion chamber at or above the hourly average temperature established for the corresponding 1-hour period of the cycle during the most recent performance test.</p>	<p>i. Measuring and recording the thermal oxidizer combustion chamber temperature at least every 15 minutes; and                      ii. Calculating the hourly average thermal oxidizer combustion chamber temperature; and                      iii. From the start of each batch cycle until 3 hours have passed since the process unit reached maximum temperature, maintaining the hourly average operating temperature in the thermal oxidizer combustion chamber at or above the minimum allowable operating temperature established for the corresponding period during the most recent performance test, as determined according to item 11 of Table 4 to this subpart; and                      iv. For each subsequent hour of the batch cycle, maintaining the hourly average operating temperature in the thermal oxidizer combustion chamber at or above the minimum allowable operating temperature established for the corresponding hour during the most recent performance test, as specified in item 13 of Table 4 to this subpart; and                      v. Reporting, in accordance with §63.9814(e), any temperature measurements below the minimum allowable thermal oxidizer combustion chamber temperature measured during the most recent performance test.</p>

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For . . .	For the following operating limit . . .	You must demonstrate continuous compliance by . . .
<p>9. Batch process units that are equipped with a catalytic oxidizer.</p>	<p>Maintain the hourly average temperature at the inlet of the catalyst bed at or above the corresponding hourly average temperature established for the corresponding 1-hour period of the cycle during the most recent performance test.</p>	<p>i. Measuring and recording temperatures at the inlet of the catalyst bed at least every 15 minutes; and                      ii. Calculating the hourly average temperature at the inlet of the catalyst bed; and                      iii. From the start of each batch cycle until 3 hours have passed since the process unit reached maximum temperature, maintaining the hourly average operating temperature at the inlet of the catalyst bed at or above the minimum allowable bed inlet temperature established for the corresponding period during the most recent performance test, as determined according to item 12 of Table 4 to this subpart; and                      iv. For each subsequent hour of the batch cycle, maintaining the hourly average operating temperature at the inlet of the catalyst bed at or above the minimum allowable bed inlet temperature established for the corresponding hour during the most recent performance test, as specified in item 13 of Table 4 to this subpart; and                      v. Reporting, in accordance with §63.9814(e), any catalyst bed inlet temperature measurements below the minimum allowable bed inlet temperature measured during the most recent performance test; and                      vi. Checking the activity level of the catalyst at least every 12 months and taking any necessary corrective action, such as replacing the catalyst, to ensure that the catalyst is performing as designed.</p>
<p>10. Each new kiln that is used to process clay refractory products.</p>	<p>As specified in items 11 through 13 of this table.</p>	<p>Satisfying the applicable requirements specified in items 11 through 13 of this table.</p>
<p>11. Each new kiln that is equipped a DLA</p>	<p>a. Maintain the average pressure drop across the DLA for each 3-hour block period at or above the minimum pressure drop established during the most recent performance test.</p> <p>b. Maintain free-flowing limestone in the feed hopper, silo, and DLA.</p> <p>c. Maintain the limestone feeder setting at or above the level established during the most recent performance test.</p> <p>d. Use the same grade of limestone from the same source as was used during the most recent performance test.</p>	<p>i. Collecting the DLA pressure drop data, as specified in item 18.a. of Table 4 to this subpart; and                      ii. Reducing the DLA pressure drop data to 1-hour and 3-hour block averages; and                      iii. Maintaining the 3-hour block average pressure drop across the DLA at or above the minimum pressure drop established during the most recent performance test.</p> <p>Verifying that the limestone hopper has an adequate amount of free-flowing limestone by performing a daily visual check of the limestone hopper.</p> <p>Recording the limestone feeder setting at least daily to verify that the feeder setting is being maintained at or above the level established during the most recent performance test.</p> <p>Using the same grade of limestone as was used during the most recent performance test and maintaining records of the source and grade of limestone.</p>

For . . .	For the following operating limit . . .	You must demonstrate continuous compliance by . . .
<p>12. Each new kiln that is equipped with a DIFF or DLS/FF.</p>	<p>a. Initiate corrective action within 1 hour of a bag leak detection system alarm and complete corrective actions in accordance with the OM&amp;M plan; AND operate and maintain the fabric filter such that the alarm does not engage for more than 5 percent of the total operating time in a 6-month block reporting period.</p> <p>b. Maintain free-flowing lime in the feed hopper or silo at all times for continuous injection systems; AND maintain feeder setting at or above the level established during the most recent performance test for continuous injection systems.</p>	<p>i. Initiating corrective action within 1 hour of a bag leak detection system alarm and completing corrective actions in accordance with the OM&amp;M plan; and</p> <p>ii. Operating and maintaining the fabric filter such that the alarm does not engage for more than 5 percent of the total operating time in a 6-month block reporting period; in calculating this operating time fraction, if inspection of the fabric filter demonstrates that no corrective action is required, no alarm time is counted; if corrective action is required, each alarm shall be counted as a minimum of 1 hour; if you take longer than 1 hour to initiate corrective action, the alarm time shall be counted as the actual amount of time taken by you to initiate corrective action.</p> <p>i. Verifying at least once each 8-hour shift that lime is free-flowing via a load cell, carrier gas/lime flow indicator, carrier gas pressure drop measurement system, or other system; recording all monitor or sensor output, and if lime is found not to be free flowing, promptly initiating and completing corrective actions; and</p> <p>ii. Recording the feeder setting once each day of operation to verify that the feeder setting is being maintained at or above the level established during the most recent performance test.</p>
<p>13. Each new kiln that is used to process clay refractory products and is equipped with a wet scrubber.</p>	<p>a. Maintain the average pressure drop across the scrubber for each 3-hour block period at or above the minimum pressure drop established during the most recent performance test.</p> <p>b. Maintain the average scrubber liquid pH for each 3-hour block period at or above the minimum scrubber liquid pH established during the most recent performance test.</p> <p>c. Maintain the average scrubber liquid flow rate for each 3-hour block period at or above the minimum scrubber liquid flow rate established during the most recent performance test.</p> <p>d. If chemicals are added to the scrubber liquid, maintain the average scrubber chemical feed rate for each 3-hour block period at or above the minimum scrubber chemical feed rate established during the most recent performance test.</p>	<p>i. Collecting the scrubber pressure drop data, as specified in item 20.a. of Table 4 to this subpart; and</p> <p>ii. Reducing the scrubber pressure drop data to 1-hour and 3-hour block averages; and</p> <p>iii. Maintaining the 3-hour block average scrubber pressure drop at or above the minimum pressure drop established during the most recent performance test.</p> <p>i. Collecting the scrubber liquid pH data, as specified in item 20.b. of Table 4 to this subpart; and</p> <p>ii. Reducing the scrubber liquid pH data to 1-hour and 3-hour block averages; and</p> <p>iii. Maintaining the 3-hour block average scrubber liquid pH at or above the minimum scrubber liquid pH established during the most recent performance test.</p> <p>i. Collecting the scrubber liquid flow rate data, as specified in item 20.c. of Table 4 to this subpart; and</p> <p>ii. Reducing the scrubber liquid flow rate data to 1-hour and 3-hour block averages; and</p> <p>iii. Maintaining the 3-hour block average scrubber liquid flow rate at or above the minimum scrubber liquid flow rate established during the most recent performance test.</p> <p>i. Collecting the scrubber chemical feed rate data, as specified in item 20.d. of Table 4 to this subpart; and</p> <p>ii. Reducing the scrubber chemical feed rate data to 1-hour and 3-hour block averages; and</p>

For . . .	For the following operating limit . . .	You must demonstrate continuous compliance by . . .
		iii. Maintaining the 3-hour block average scrubber chemical feed rate at or above the minimum scrubber chemical feed rate established during the most recent performance test.

TABLE 9 TO SUBPART SSSSS OF PART 63—CONTINUOUS COMPLIANCE WITH WORK PRACTICE STANDARDS

As stated in §63.9810, you must show continuous compliance with the work practice standards for affected sources according to the following table:

For . . .	For the following work practice standard . . .	You must demonstrate continuous compliance by . . .
1. Each affected source listed in Table 3 to this subpart.	Each applicable work practice requirement listed in Table 3 to this subpart.	<ul style="list-style-type: none"> <li>i. Performing each applicable work practice standard listed in Table 3 to this subpart; and</li> <li>ii. Maintaining records that document the method and frequency for complying with each applicable work practice standard listed in Table 3 to this subpart, as required by §§63.10(b) and 63.9816(c)(2).</li> </ul>
2. Each basket or container that is used for holding fired refractory shapes in an existing shape preheater and autoclave during the pitch impregnation process.	Control POM emissions from any affected shape preheater.	<ul style="list-style-type: none"> <li>i. Controlling emissions from the volatilization of residual pitch by implementing one of the work practice standards listed in item 1 of Table 3 to this subpart; and</li> <li>ii. Recording the date and cleaning method each time you clean an affected basket or container.</li> </ul>
3. Each new or existing pitch working tank	Control POM emissions .....	Capturing and venting emissions from the affected pitch working tank to the control device that is used to control emissions from an affected defumer or coking oven, or to a thermal or catalytic oxidizer that is comparable to the control device used on an affected defumer or coking oven.
4. Each new or existing chromium refractory products kiln.	Minimize fuel-based HAP emissions .....	<ul style="list-style-type: none"> <li>i. Using natural gas, or equivalent, as the kiln fuel at all times except during periods of natural gas curtailment or supply interruption; and</li> <li>ii. If you intend to use an alternative fuel, submitting a notification of alternative fuel use within 48 hours of the declaration of a period of natural gas curtailment or supply interruption, as defined in §63.9824; and</li> <li>iii. Submitting a report of alternative fuel use within 10 working days after terminating the use of the alternative fuel, as specified in §63.9814(g).</li> </ul>
5. Each existing clay refractory products kiln.	Minimize fuel-based HAP emissions .....	<ul style="list-style-type: none"> <li>i. Using natural gas, or equivalent, as the kiln fuel at all times except during periods of natural gas curtailment or supply interruption; and</li> <li>ii. If you intend to use an alternative fuel, submitting a notification of alternative fuel use within 48 hours of the declaration of a period of natural gas curtailment or supply interruption, as defined in §63.9824; and</li> <li>iii. Submitting a report of alternative fuel use within 10 working days after terminating the use of the alternative fuel, as specified in §63.9814(g).</li> </ul>

TABLE 10 TO SUBPART SSSSS OF PART 63—REQUIREMENTS FOR REPORTS

As stated in §63.9814, you must comply with the requirements for reports in the following table:

You must submit a(n) . . .	The report must contain . . .	You must submit the report . . .
1. Compliance report .....	The information in §63.9814(c) through (f).	Semiannually according to the requirements in §63.9814(a) through (f).
2. Immediate startup, shutdown, and malfunction report if you had a startup, shutdown, or malfunction during the reporting period that is not consistent with your SSMP.	a. Actions taken for the event .....	By fax or telephone within 2 working days after starting actions inconsistent with the plan.
	b. The information in §63.10(d)(5)(ii) .....	By letter within 7 working days after the end of the event unless you have made alternative arrangements with the permitting authority.
3. Report of alternative fuel use .....	The information in §63.9814(g) and items 4 and 5 of Table 9 to this subpart.	If you are subject to the work practice standard specified in item 3 or 4 of Table 3 to this subpart, and you use an alternative fuel in the affected kiln, by letter within 10 working days after terminating the use of the alternative fuel.

TABLE 11 TO SUBPART SSSSS OF PART 63—APPLICABILITY OF GENERAL PROVISIONS TO SUBPART SSSSS

As stated in §63.9820, you must comply with the applicable General Provisions requirements according to the following table:

Citation	Subject	Brief description	Applies to subpart SSSSS
§ 63.1 .....	Applicability .....	.....	Yes.
§ 63.2 .....	Definitions .....	.....	Yes.
§ 63.3 .....	Units and Abbreviations .....	.....	Yes.
§ 63.4 .....	Prohibited Activities .....	Compliance date; circumvention, severity.	Yes.
§ 63.5 .....	Construction/Reconstruction .....	Applicability; applications; approvals .....	Yes.
§ 63.6(a) .....	Applicability .....	General Provisions (GP) apply unless compliance extension; GP apply to area sources that become major.	Yes.
§ 63.6(b)(1)–(4) ..	Compliance Dates for New and Reconstructed Sources.	Standards apply at effective date; 3 years after effective date; upon startup; 10 years after construction or reconstruction commences for section 112(f).	Yes.
§ 63.6(b)(5) .....	Notification .....	.....	Yes.
§ 63.6(b)(6) .....	[Reserved]		
§ 63.6(b)(7) .....	Compliance Dates for New and Reconstructed Area Sources That Become Major.	Area sources that become major must comply with major source standards immediately upon becoming major, regardless of whether required to comply when they were area sources.	Yes.
§ 63.6(c)(1)–(2) ..	Compliance Dates for Existing Sources ...	Comply according to date in subpart, which must be no later than 3 years after effective date; for section 112(f) standards, comply within 90 days of effective date unless compliance extension.	Yes.
§ 63.6(c)(3)–(4) ..	[Reserved]		
§ 63.6(c)(5) .....	Compliance Dates for Existing Area Sources That Become Major.	Area sources that become major must comply with major source standards by date indicated in subpart or by equivalent time period (for example, 3 years).	Yes.
§ 63.6(d) .....	[Reserved]		
§ 63.6(e)(1)–(2) ..	Operation & Maintenance .....	Operate to minimize emissions at all times; correct malfunctions as soon as practicable; requirements independently enforceable; information Administrator will use to determine if operation and maintenance requirements were met.	Yes.

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Citation	Subject	Brief description	Applies to subpart SSSSS
§ 63.6(e)(3) .....	Startup, Shutdown, and Malfunction Plan (SSMP) .....	.....	Yes.
§ 63.6(f)(1) .....	Compliance Except During SSM .....	You must comply with emission standards at all times except during SSM.	Yes.
§ 63.6(f)(2)–(3) ..	Methods for Determining Compliance .....	Compliance based on performance test, operation and maintenance plans, records, inspection.	Yes.
§ 63.6(g)(1)–(3) ..	Alternative Standard .....	Procedures for getting an alternative standard.	Yes.
§ 63.6(h)(1)–(9) ..	Opacity/Visible Emission (VE) Standards .....	.....	Not applicable.
§ 63.6(i)(1)–(14)	Compliance Extension .....	Procedures and criteria for Administrator to grant compliance extension.	Yes.
§ 63.6(j) .....	Presidential Compliance Exemption .....	President may exempt source category ...	Yes.
§ 63.7(a)(1)–(2) ..	Performance Test Dates .....	Dates for conducting initial performance testing and other compliance demonstrations; must conduct 180 days after first subject to rule.	Yes.
§ 63.7(a)(3) .....	Section 114 Authority .....	Administrator may require a performance test under CAA section 114 at any time.	Yes.
§ 63.7(b)(1) .....	Notification of Performance Test .....	Must notify Administrator 60 days before the test.	Yes.
§ 63.7(b)(2) .....	Notification of Rescheduling .....	Must notify Administrator 5 days before scheduled date and provide rescheduled date.	Yes.
§ 63.7(c) .....	Quality Assurance/Test Plan .....	Requirements; test plan approval procedures; performance audit requirements; internal and external QA procedures for testing.	Yes.
§ 63.7(d) .....	Testing Facilities .....	.....	Yes.
§ 63.7(e)(1) .....	Conditions for Conducting Performance Tests.	Performance tests must be conducted under representative conditions; cannot conduct performance tests during SSM; not a violation to exceed standard during SSM.	No, § 63.9800 specifies requirements; Yes; Yes.
§ 63.7(e)(2) .....	Conditions for Conducting Performance Tests.	Must conduct according to subpart and EPA test methods unless Administrator approves alternative.	Yes.
§ 63.7(e)(3) .....	Test Run Duration .....	Must have three test runs of at least 1 hour each; compliance is based on arithmetic mean of three runs; conditions when data from an additional test run can be used.	Yes; Yes, except where specified in § 63.9800 for batch process sources; Yes.
§ 63.7(f) .....	Alternative Test Method .....	.....	Yes.
§ 63.7(g) .....	Performance Test Data Analysis .....	.....	Yes.
§ 63.7(h) .....	Waiver of Test .....	.....	Yes.
§ 63.8(a)(1) .....	Applicability of Monitoring Requirements .....	.....	Yes.
§ 63.8(a)(2) .....	Performance Specifications .....	Performance Specifications in appendix B of 40 CFR part 60 apply.	Yes.
§ 63.8(a)(3) .....	[Reserved]	.....	.....
§ 63.8(a)(4) .....	Monitoring with Flares .....	.....	Not applicable.
§ 63.8(b)(1) .....	Monitoring .....	Must conduct monitoring according to standard unless Administrator approves alternative.	Yes.
§ 63.8(b)(2)–(3) ..	Multiple Effluents and Multiple Monitoring Systems.	Specific requirements for installing and reporting on monitoring systems.	Yes.
§ 63.8(c)(1) .....	Monitoring System Operation and Maintenance.	Maintenance consistent with good air pollution control practices.	Yes.
§ 63.8(c)(1)(i) .....	Routine and Predictable SSM .....	Reporting requirements for SSM when action is described in SSMP.	Yes.
§ 63.8(c)(1)(ii) .....	SSM not in SSMP .....	Reporting requirements for SSM when action is not described in SSMP.	Yes.
§ 63.8(c)(1)(iii) .....	Compliance with Operation and Maintenance Requirements.	How Administrator determines if source is complying with operation and maintenance requirements.	Yes.
§ 63.8(c)(2)–(3) ..	Monitoring System Installation .....	Must install to get representative emission and parameter measurements.	Yes.
§ 63.8(c)(4) .....	CMS Requirements .....	.....	No, § 63.9808 specifies requirements.
§ 63.8(c)(5) .....	COMS Minimum Procedures .....	.....	Not applicable.
§ 63.8(c)(6) .....	CMS Requirements .....	.....	Applies only to sources required to install and operate a THC CEMS.

Citation	Subject	Brief description	Applies to subpart SSSSS
§ 63.8(c)(7)(i)(A)	CMS Requirements .....	.....	Applies only to sources required to install and operate a THC CEMS.
§ 63.8(c)(7)(i)(B)	CMS Requirements .....	.....	Applies only to sources required to install and operate a THC CEMS.
§ 63.8(c)(7)(i)(C)	CMS Requirements .....	.....	Not applicable.
§ 63.8(c)(7)(ii) ....	CMS Requirements .....	Corrective action required when CMS is out of control.	Yes.
§ 63.8(c)(8) .....	CMS Requirements .....	.....	Yes.
§ 63.8(d) .....	CMS Quality Control .....	.....	Applies only to sources required to install and operate a THC CEMS.
§ 63.8(e) .....	CMS Performance Evaluation .....	.....	Applies only to sources required to install and operate a THC CEMS.
§ 63.8(f)(1)–(5) ..	Alternative Monitoring Method .....	.....	Yes.
§ 63.8(f)(6) .....	Alternative to Relative Accuracy Test .....	.....	Yes.
§ 63.8(g) .....	Data Reduction .....	.....	Applies only to sources required to install and operate a THC CEMS.
§ 63.9(a) .....	Notification Requirements .....	.....	Yes.
§ 63.9(b)(1)–(5) ..	Initial Notifications .....	.....	Yes.
§ 63.9(c) .....	Request for Compliance Extension .....	.....	Yes.
§ 63.9(d) .....	Notification of Special Compliance Requirements for New Source.	.....	Yes.
§ 63.9(e) .....	Notification of Performance Test .....	Notify Administrator 60 days prior .....	Yes.
§ 63.9(f) .....	Notification of VE/Opacity Test .....	.....	Not applicable.
§ 63.9(g) .....	Additional Notifications When Using CMS	.....	Applies only to sources required to install and operate a THC CEMS.
§ 63.9(h) .....	Notification of Compliance Status .....	.....	Yes.
§ 63.9(i) .....	Adjustment of Submittal Deadlines .....	.....	Yes.
§ 63.9(j) .....	Change in Previous Information .....	.....	Yes.
§ 63.10(a) .....	Recordkeeping/Reporting .....	.....	Yes.
§ 63.10(b)(1) ....	Recordkeeping/Reporting .....	.....	Yes.
§ 63.10(b)(2)(i)–(v).	Records Related to Startup, Shutdown, and Malfunction.	.....	Yes.
§ 63.10(b)(2)(vi) and (x–xi).	CMS Records .....	.....	Yes.
§ 63.10(b)(2)(vii)–(ix).	Records .....	Measurements to demonstrate compliance with emission limitations; performance test, performance evaluation, and visible emission observation results; measurements to determine conditions of performance tests and performance evaluations.	Yes.
§ 63.10(b)(2)(xii)	Records .....	Records when under waiver .....	Yes.
§ 63.10(b)(2)(xiii)	Records .....	Records when using alternative to relative accuracy test.	Not applicable.
§ 63.10(b)(2)(xiv)	Records .....	All documentation supporting Initial Notification and Notification of Compliance Status.	Yes.
§ 63.10(b)(3) ....	Records .....	Applicability Determinations .....	Yes.
§ 63.10(c)(1)–(6), (9)–(15).	Records .....	Additional Records for CMS .....	Not applicable.
§ 63.10(c)(7)–(8)	Records .....	Records of excess emissions and parameter monitoring exceedances for CMS.	No, § 63.9816 specifies requirements.
§ 63.10(d)(1) ....	General Reporting Requirements .....	Requirements for reporting .....	Yes.
§ 63.10(d)(2) ....	Report of Performance Test Results .....	When to submit to Federal or State authority.	Yes.
§ 63.10(d)(3) ....	Reporting Opacity or VE Observations .....	.....	Not applicable.
§ 63.10(d)(4) ....	Progress Reports .....	Must submit progress reports on schedule if under compliance extension.	Yes.
§ 63.10(d)(5) ....	Startup, Shutdown, and Malfunction Reports.	Contents and submission .....	Yes.

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**§ 63.9883**

Citation	Subject	Brief description	Applies to subpart SSSS
§ 63.10(e)(1)–(2)	Additional CMS Reports .....	.....	Applies only to sources required to install and operate a THC CEMS.
§ 63.10(e)(3) .....	Reports .....	.....	No, § 63.9814 specifies requirements.
§ 63.10(e)(4) .....	Reporting COMS data .....	.....	Not applicable.
§ 63.10(f) .....	Waiver for Recordkeeping/Reporting .....	.....	Yes.
§ 63.11 .....	Flares .....	.....	Not applicable.
§ 63.12 .....	Delegation .....	.....	Yes.
§ 63.13 .....	Addresses .....	.....	Yes.
§ 63.14 .....	Incorporation by Reference .....	.....	Yes.
§ 63.15 .....	Availability of Information .....	.....	Yes.

**Subpart TTTT—National Emissions Standards for Hazardous Air Pollutants for Primary Magnesium Refining**

SOURCE: 68 FR 58620, Oct. 10, 2003, unless otherwise noted.

**WHAT THIS SUBPART COVERS**

**§ 63.9880 What is the purpose of this subpart?**

This subpart establishes national emission standards for hazardous air pollutants (NESHAP) for primary magnesium refineries. This subpart also establishes requirements to demonstrate initial and continuous compliance with all applicable emission limitations, work practice standards, and operation and maintenance requirements.

**§ 63.9881 Am I subject to this subpart?**

You are subject to this subpart if you own or operate a primary magnesium refinery that is (or is part of) a major source of hazardous air pollutant (HAP) emissions. Your primary magnesium refinery is a major source of HAP if it emits or has the potential to emit any single HAP at a rate of 10 tons or more per year or any combination of HAP at a rate of 25 tons or more per year.

**§ 63.9882 What parts of my plant does this subpart cover?**

- (a) The affected sources are each new and existing primary magnesium refining facility.
- (b) This subpart covers emissions from each spray dryer stack, magnesium chloride storage bins scrubber stack, melt/reactor system stack, and

launder off-gas system stack at your primary magnesium refining facility. This subpart also covers fugitive dust emissions.

(c) Each primary magnesium refining facility is existing if you commenced construction or reconstruction of the affected source before January 22, 2003.

(d) Each primary magnesium refining facility is new if you commence construction or reconstruction of the affected source on or after January 22, 2003. An affected source is reconstructed if it meets the definition of reconstruction in § 63.2.

**§ 63.9883 When do I have to comply with this subpart?**

(a) If you have an existing source, you must comply with each emission limitation, work practice standard, and operation and maintenance requirement in this subpart that applies to you no later than October 11, 2004.

(b) If you have a new affected source and its initial startup date is on or before October 11, 2003, you must comply with each emission limitation, work practice standard, and operation and maintenance requirement in this subpart that applies to you by October 10, 2003.

(c) If you have a new affected source and its initial startup date is after October 10, 2003, you must comply with each emission limitation, work practice standard, and operation and maintenance requirement in this subpart that applies to you upon initial startup.

(d) If your primary magnesium refinery is an area source that becomes a major source of HAP, the compliance